

Ene-47.124 Höyrykattilatekniikka (2 ov)

Tentti - la 10.12.2005

Tentissä on 5 tehtävää ja maksimi pistemäärä on 20.

1. (5p)

Piirrä polypolttokattilan periaatekuva, johon nimeät eri lämmönsiirtopinta-alat. Esitä saman kattilan T_s - ja T_c piirroksat ja kirjoita näihin kuviin lämmönsiirtopinta-alat.

2. (3p)

Määritä kattilan hyötysuhde ja luettele suurimmat häviötekijät.

3. (3p)

Kattiloita voidaan jakaa eri tyyppeihin vesikierron perusteella. Piirrä periaatekuvat näistä ja selitä miten vesikierto niissä toimii.

4. (5p)

Höyrykattila tuottaa 12 t/h höyryä, jonka lämpötila on 250°C ja paine 20 bar. Polttoaineena käytettävää hiiltä (tehollinen lämpöarvo $H_i = 28 \text{ MJ/kg}$) kuluu 1.46 t/h. Syöttöveden lämpötila on 32°C, ekonomaisesta lähtevän veden lämpötila on 120°C ja höyrystimestä lähtevän vesi-höyryseoksen höyrypitoisuus $x = 0.95$. Veden/höyryn paine oletetaan samaksi kaikissa kattilan osissa. Palamisen hyötysuhde kattilassa on 90 %. Polttoilmaa tarvitaan 8 normi-m³/kg polttoainetta ja lämpötilassa 20°C prosessiin sisään otettu ilma lämmitetään lämpötilaan 85°C.

Laske:

- a) Kuinka suuri osa polttoaineen mukana prosessiin tuodusta lämmöstä käytetään
- ekonomaisierissa
 - höyrystimestä
 - tulistimessa
 - ilman esilämmittimessä ? (3p)
- b) Mikä on kattilan hyötysuhde (2p) ?

5. (4p)

Polttoaineen alkuaineanalyysi massaprosentteina on:

| | |
|----------------|----------|
| C | = 78,0 % |
| H ₂ | = 4,5 % |
| S | = 1,5 % |
| O ₂ | = 6,0 % |
| tuhka | = 10,0 % |

Laske:

- a)** Todelliset ilma- ja savukaasumäärät, kun palaminen tapahtuu 20 % ilmaylimäärällä. (2p)
- b)** Savukaasujen koostumus. Anna tulokset muodossa kg/kg polttoainetta. (2p)

TABLE A-3 Properties of Saturated Water (Liquid-Vapor): Pressure Table

| Press. bars | Temp. °C | Specific Volume m ³ /kg | | Internal Energy kJ/kg | | Enthalpy kJ/kg | | | Entropy kJ/kg · K | | Press. bars |
|-------------|----------|------------------------------------|------------------|-----------------------|------------------|-------------------|----------------|------------------|-------------------|------------------|-------------|
| | | Sat. Liquid $v_f \times 10^3$ | Sat. Vapor v_g | Sat. Liquid u_f | Sat. Vapor u_g | Sat. Liquid h_f | Evap. h_{fg} | Sat. Vapor h_g | Sat. Liquid s_f | Sat. Vapor s_g | |
| 0.04 | 28.96 | 1.0040 | 34.800 | 121.45 | 2415.2 | 121.46 | 2432.9 | 2554.4 | 0.4226 | 8.4746 | 0.04 |
| 0.06 | 36.16 | 1.0064 | 23.739 | 151.53 | 2425.0 | 151.53 | 2415.9 | 2567.4 | 0.5210 | 8.3304 | 0.06 |
| 0.08 | 41.51 | 1.0084 | 18.103 | 173.87 | 2432.2 | 173.88 | 2403.1 | 2577.0 | 0.5926 | 8.2287 | 0.08 |
| 0.10 | 45.81 | 1.0102 | 14.674 | 191.82 | 2437.9 | 191.83 | 2392.8 | 2584.7 | 0.6493 | 8.1502 | 0.10 |
| 0.20 | 60.06 | 1.0172 | 7.649 | 251.38 | 2456.7 | 251.40 | 2358.3 | 2609.7 | 0.8320 | 7.9085 | 0.20 |
| 0.30 | 69.10 | 1.0223 | 5.229 | 289.20 | 2468.4 | 289.23 | 2336.1 | 2625.3 | 0.9439 | 7.7686 | 0.30 |
| 0.40 | 75.87 | 1.0265 | 3.993 | 317.53 | 2477.0 | 317.58 | 2319.2 | 2636.8 | 1.0259 | 7.6700 | 0.40 |
| 0.50 | 81.33 | 1.0300 | 3.240 | 340.44 | 2483.9 | 340.49 | 2305.4 | 2645.9 | 1.0910 | 7.5939 | 0.50 |
| 0.60 | 85.94 | 1.0331 | 2.732 | 359.79 | 2489.6 | 359.86 | 2293.6 | 2653.5 | 1.1453 | 7.5320 | 0.60 |
| 0.70 | 89.95 | 1.0360 | 2.365 | 376.63 | 2494.5 | 376.70 | 2283.3 | 2660.0 | 1.1919 | 7.4797 | 0.70 |
| 0.80 | 93.50 | 1.0380 | 2.087 | 391.58 | 2498.8 | 391.66 | 2274.1 | 2665.8 | 1.2329 | 7.4346 | 0.80 |
| 0.90 | 96.71 | 1.0410 | 1.869 | 405.06 | 2502.6 | 405.15 | 2265.7 | 2670.9 | 1.2695 | 7.3949 | 0.90 |
| 1.00 | 99.63 | 1.0432 | 1.694 | 417.36 | 2506.1 | 417.46 | 2258.0 | 2675.5 | 1.3026 | 7.3594 | 1.00 |
| 1.50 | 111.4 | 1.0528 | 1.159 | 466.94 | 2519.7 | 467.11 | 2226.5 | 2693.6 | 1.4336 | 7.2233 | 1.50 |
| 2.00 | 120.2 | 1.0605 | 0.8857 | 504.49 | 2529.5 | 504.70 | 2201.9 | 2706.7 | 1.5301 | 7.1271 | 2.00 |
| 2.50 | 127.4 | 1.0672 | 0.7187 | 535.10 | 2537.2 | 535.37 | 2181.5 | 2716.9 | 1.6072 | 7.0527 | 2.50 |
| 3.00 | 133.6 | 1.0732 | 0.6058 | 561.15 | 2543.6 | 561.47 | 2163.8 | 2725.3 | 1.6718 | 6.9919 | 3.00 |
| 3.50 | 138.9 | 1.0786 | 0.5243 | 583.95 | 2546.9 | 584.33 | 2148.1 | 2732.4 | 1.7275 | 6.9405 | 3.50 |
| 4.00 | 143.6 | 1.0836 | 0.4625 | 604.31 | 2553.6 | 604.74 | 2133.8 | 2738.6 | 1.7766 | 6.8959 | 4.00 |
| 4.50 | 147.9 | 1.0882 | 0.4140 | 622.25 | 2557.6 | 623.25 | 2120.7 | 2743.9 | 1.8207 | 6.8565 | 4.50 |
| 5.00 | 151.9 | 1.0926 | 0.3749 | 639.68 | 2561.2 | 640.23 | 2108.5 | 2748.7 | 1.8607 | 6.8212 | 5.00 |
| 6.00 | 158.9 | 1.1006 | 0.3157 | 669.90 | 2567.4 | 670.56 | 2086.3 | 2756.8 | 1.9312 | 6.7600 | 6.00 |
| 7.00 | 165.0 | 1.1080 | 0.2729 | 696.44 | 2572.5 | 697.22 | 2066.3 | 2763.5 | 1.9922 | 6.7080 | 7.00 |
| 8.00 | 170.4 | 1.1148 | 0.2404 | 720.22 | 2576.8 | 721.11 | 2048.0 | 2769.1 | 2.0462 | 6.6628 | 8.00 |
| 9.00 | 175.4 | 1.1212 | 0.2150 | 741.83 | 2580.5 | 742.83 | 2031.1 | 2773.9 | 2.0946 | 6.6226 | 9.00 |
| 10.0 | 179.9 | 1.1273 | 0.1944 | 761.68 | 2583.6 | 762.81 | 2015.3 | 2778.1 | 2.1387 | 6.5863 | 10.0 |
| 15.0 | 198.3 | 1.1539 | 0.1318 | 843.16 | 2594.5 | 844.84 | 1947.3 | 2792.2 | 2.3150 | 6.4448 | 15.0 |
| 20.0 | 212.4 | 1.1767 | 0.09963 | 906.44 | 2600.3 | 908.79 | 1890.7 | 2799.5 | 2.4474 | 6.3409 | 20.0 |
| 25.0 | 224.0 | 1.1973 | 0.07998 | 959.11 | 2603.1 | 962.11 | 1841.0 | 2803.1 | 2.5547 | 6.2575 | 25.0 |
| 30.0 | 233.9 | 1.2165 | 0.06668 | 1004.8 | 2604.1 | 1008.4 | 1795.7 | 2804.2 | 2.6457 | 6.1869 | 30.0 |
| 35.0 | 242.6 | 1.2347 | 0.05707 | 1045.4 | 2603.7 | 1049.8 | 1753.7 | 2803.4 | 2.7253 | 6.1253 | 35.0 |
| 40.0 | 250.4 | 1.2522 | 0.04978 | 1082.3 | 2602.3 | 1087.3 | 1714.1 | 2801.4 | 2.7964 | 6.0701 | 40.0 |
| 45.0 | 257.5 | 1.2692 | 0.04406 | 1116.2 | 2600.1 | 1121.9 | 1676.4 | 2798.3 | 2.8610 | 6.0199 | 45.0 |
| 50.0 | 264.0 | 1.2859 | 0.03944 | 1147.8 | 2597.1 | 1154.2 | 1640.1 | 2794.3 | 2.9202 | 5.9734 | 50.0 |
| 60.0 | 275.6 | 1.3187 | 0.03244 | 1205.4 | 2589.7 | 1213.4 | 1571.0 | 2784.3 | 3.0267 | 5.8892 | 60.0 |
| 70.0 | 285.9 | 1.3513 | 0.02737 | 1257.6 | 2580.5 | 1267.0 | 1505.1 | 2772.1 | 3.1211 | 5.8133 | 70.0 |
| 80.0 | 295.1 | 1.3842 | 0.02352 | 1305.6 | 2569.8 | 1316.6 | 1441.3 | 2758.0 | 3.2068 | 5.7432 | 80.0 |
| 90.0 | 303.4 | 1.4178 | 0.02048 | 1350.5 | 2557.8 | 1363.3 | 1378.9 | 2742.1 | 3.2858 | 5.6772 | 90.0 |
| 100. | 311.1 | 1.4524 | 0.01803 | 1393.0 | 2544.4 | 1407.6 | 1317.1 | 2724.7 | 3.3596 | 5.6141 | 100. |
| 110. | 318.2 | 1.4886 | 0.01599 | 1433.7 | 2529.8 | 1450.1 | 1255.5 | 2705.6 | 3.4295 | 5.5527 | 110. |

TABLE A-4 Properties of Superheated Water Vapor

| T °C | v m ³ /kg | h kJ/kg | u kJ/kg | s kJ/kg · K | v m ³ /kg | h kJ/kg | u kJ/kg | s kJ/kg · K |
|-----------|---------------------------|--------------|--------------|------------------|---------------------------|--------------|--------------|------------------|
| Sat. | 23.739 | 2425.0 | 2567.4 | 8.3304 | 4.526 | 2473.0 | 2631.4 | 7.158 |
| 80 | 27.132 | 2487.3 | 2650.1 | 8.5804 | 4.625 | 2483.7 | 2645.6 | 7.764 |
| 120 | 30.219 | 2544.7 | 2726.0 | 8.7840 | 5.163 | 2542.4 | 2723.1 | 7.9644 |
| 160 | 33.302 | 2603.7 | 2802.5 | 8.9693 | 5.696 | 2601.2 | 2800.6 | 8.1519 |
| 200 | 36.383 | 2661.4 | 2879.7 | 9.1398 | 6.228 | 2660.4 | 2878.4 | 8.2327 |
| 240 | 39.462 | 2721.0 | 2957.8 | 9.2982 | 6.758 | 2720.3 | 2956.8 | 8.4828 |
| 280 | 42.540 | 2781.5 | 3036.8 | 9.4464 | 7.287 | 2780.9 | 3036.0 | 8.6314 |
| 320 | 45.618 | 2843.0 | 3116.7 | 9.5859 | 7.815 | 2842.5 | 3116.1 | 8.7712 |
| 360 | 48.696 | 2905.5 | 3197.7 | 9.7180 | 8.344 | 2905.1 | 3197.1 | 8.9034 |
| 400 | 51.774 | 2969.0 | 3279.6 | 9.8335 | 8.872 | 2968.6 | 3279.2 | 9.0291 |
| 440 | 54.851 | 3033.5 | 3362.6 | 9.9633 | 9.400 | 3033.2 | 3362.2 | 9.1490 |
| 500 | 59.467 | 3132.3 | 3489.1 | 10.1336 | 10.192 | 3132.1 | 3488.8 | 9.3194 |

$p = 0.06 \text{ bar} = 0.006 \text{ MPa}$
($T_{\text{sat}} = 36.16^\circ\text{C}$)

$p = 0.07 \text{ bar} = 0.007 \text{ MPa}$
($T_{\text{sat}} = 89.95^\circ\text{C}$)

$p = 0.10 \text{ bar} = 0.010 \text{ MPa}$
($T_{\text{sat}} = 99.63^\circ\text{C}$)

$p = 1.0 \text{ bar} = 0.10 \text{ MPa}$
($T_{\text{sat}} = 179.91^\circ\text{C}$)

$p = 1.5 \text{ bars} = 0.15 \text{ MPa}$
($T_{\text{sat}} = 111.37^\circ\text{C}$)

$p = 3.0 \text{ bars} = 0.30 \text{ MPa}$
($T_{\text{sat}} = 133.55^\circ\text{C}$)

| T °C | v m ³ /kg | h kJ/kg | u kJ/kg | s kJ/kg · K | v m ³ /kg | h kJ/kg | u kJ/kg | s kJ/kg · K |
|-----------|---------------------------|--------------|--------------|------------------|---------------------------|--------------|--------------|------------------|
| Sat. | 0.3749 | 2561.2 | 2748.7 | 6.8213 | 0.2799 | 2567.5 | 2792.2 | 6.4448 |
| 180 | 0.4045 | 2609.7 | 2812.0 | 6.9656 | 0.2847 | 2599.8 | 2799.1 | 6.7880 |
| 200 | 0.4249 | 2642.9 | 2855.4 | 7.0592 | 0.2999 | 2634.8 | 2844.8 | 6.8865 |
| 240 | 0.4646 | 2707.6 | 2939.9 | 7.2307 | 0.3292 | 2701.8 | 2932.2 | 7.0641 |
| 280 | 0.5034 | 2771.2 | 3022.9 | 7.3865 | 0.3574 | 2766.9 | 3017.1 | 7.2233 |
| 320 | 0.5416 | 2834.7 | 3105.6 | 7.5308 | 0.3852 | 2831.3 | 3100.9 | 7.3697 |
| 360 | 0.5796 | 2898.7 | 3188.4 | 7.6660 | 0.4126 | 2895.8 | 3184.7 | 7.5063 |
| 400 | 0.6173 | 2963.2 | 3271.9 | 7.7938 | 0.4397 | 2960.9 | 3268.7 | 7.6350 |
| 440 | 0.6548 | 3028.6 | 3356.0 | 7.9152 | 0.4667 | 3026.6 | 3353.3 | 7.7571 |
| 500 | 0.7109 | 3128.4 | 3483.9 | 8.0873 | 0.5070 | 3126.8 | 3481.7 | 7.9299 |
| 600 | 0.8041 | 3299.6 | 3701.7 | 8.3522 | 0.5738 | 3298.5 | 3700.2 | 8.1956 |
| 700 | 0.8969 | 3477.5 | 3925.9 | 8.5952 | 0.6403 | 3476.6 | 3924.8 | 8.4391 |

$p = 5.0 \text{ bars} = 0.50 \text{ MPa}$
($T_{\text{sat}} = 151.86^\circ\text{C}$)

$p = 7.0 \text{ bars} = 0.70 \text{ MPa}$
($T_{\text{sat}} = 164.97^\circ\text{C}$)

$p = 10.0 \text{ bars} = 1.0 \text{ MPa}$
($T_{\text{sat}} = 179.91^\circ\text{C}$)

$p = 15.0 \text{ bars} = 1.5 \text{ MPa}$
($T_{\text{sat}} = 198.32^\circ\text{C}$)

$p = 20.0 \text{ bars} = 2.0 \text{ MPa}$
($T_{\text{sat}} = 212.42^\circ\text{C}$)

$p = 30.0 \text{ bars} = 3.0 \text{ MPa}$
($T_{\text{sat}} = 233.90^\circ\text{C}$)

TABLE A-4 (Continued)

TABLE A-14 Ideal Gas Specific Heats of Some Common Gases (kJ/kg · K)

| Temp. K | Air | | Nitrogen, N ₂ | | Oxygen, O ₂ | | Temp. K |
|------------|----------------|----------------|--------------------------|----------------|------------------------|-------|------------|
| | c _p | c _v | k | c _p | c _v | k | |
| 250 | 1.003 | 0.716 | 1.401 | 1.039 | 0.742 | 1.400 | 250 |
| 300 | 1.005 | 0.718 | 1.400 | 1.039 | 0.743 | 1.400 | 300 |
| 350 | 1.008 | 0.721 | 1.398 | 1.041 | 0.744 | 1.399 | 350 |
| 400 | 1.013 | 0.726 | 1.395 | 1.044 | 0.747 | 1.397 | 400 |
| 450 | 1.020 | 0.733 | 1.391 | 1.049 | 0.752 | 1.395 | 450 |
| 500 | 1.029 | 0.742 | 1.387 | 1.056 | 0.759 | 1.391 | 500 |
| 550 | 1.040 | 0.753 | 1.381 | 1.065 | 0.768 | 1.387 | 550 |
| 600 | 1.051 | 0.764 | 1.376 | 1.075 | 0.778 | 1.382 | 600 |
| 650 | 1.063 | 0.776 | 1.370 | 1.086 | 0.789 | 1.376 | 650 |
| 700 | 1.075 | 0.788 | 1.364 | 1.098 | 0.801 | 1.371 | 700 |
| 750 | 1.087 | 0.800 | 1.359 | 1.110 | 0.813 | 1.365 | 750 |
| 800 | 1.099 | 0.812 | 1.354 | 1.121 | 0.825 | 1.360 | 800 |
| 900 | 1.121 | 0.834 | 1.344 | 1.145 | 0.849 | 1.349 | 900 |
| 1000 | 1.142 | 0.855 | 1.336 | 1.167 | 0.870 | 1.341 | 1000 |

| Temp. K | Carbon dioxide, CO ₂ | | Carbon monoxide, CO | | Hydrogen, H ₂ | | Temp. K |
|------------|---------------------------------|----------------|---------------------|----------------|--------------------------|-------|------------|
| | c _p | c _v | k | c _p | c _v | k | |
| 250 | 0.791 | 0.602 | 1.314 | 1.039 | 0.743 | 1.400 | 250 |
| 300 | 0.846 | 0.657 | 1.288 | 1.040 | 0.744 | 1.399 | 300 |
| 350 | 0.895 | 0.706 | 1.268 | 1.043 | 0.746 | 1.398 | 350 |
| 400 | 0.939 | 0.750 | 1.252 | 1.047 | 0.751 | 1.395 | 400 |
| 450 | 0.978 | 0.790 | 1.239 | 1.054 | 0.757 | 1.392 | 450 |
| 500 | 1.014 | 0.825 | 1.229 | 1.063 | 0.767 | 1.387 | 500 |
| 550 | 1.046 | 0.857 | 1.220 | 1.075 | 0.778 | 1.382 | 550 |
| 600 | 1.075 | 0.886 | 1.213 | 1.087 | 0.790 | 1.376 | 600 |
| 650 | 1.102 | 0.913 | 1.207 | 1.100 | 0.803 | 1.370 | 650 |
| 700 | 1.126 | 0.937 | 1.202 | 1.113 | 0.816 | 1.364 | 700 |
| 750 | 1.148 | 0.959 | 1.197 | 1.126 | 0.829 | 1.358 | 750 |
| 800 | 1.169 | 0.980 | 1.193 | 1.139 | 0.842 | 1.353 | 800 |
| 900 | 1.204 | 1.015 | 1.186 | 1.163 | 0.866 | 1.343 | 900 |
| 1000 | 1.234 | 1.045 | 1.181 | 1.185 | 0.888 | 1.335 | 1000 |

Source: Adapted from K. Wark, *Thermodynamics, 4th ed.*, McGraw-Hill, New York, 1983, as based on "Tables of Thermal Properties of Gases," NBS Circular 564, 1955.

TABLE A-1 Atomic or Molecular Weights and Critical Properties of Some Common Elements and Compounds

| Substance | Chemical formula | M | T_c , K | p_c , bars | $Z_c = \frac{p_c v_c}{RT_c}$ |
|------------------|-----------------------------------|--------|-----------|--------------|------------------------------|
| Acetylene | C ₂ H ₂ | 26.04 | 309 | 62.8 | 0.274 |
| Air (equivalent) | — | 28.97 | 133 | 37.7 | 0.284 |
| Ammonia | NH ₃ | 17.04 | 406 | 112.8 | 0.242 |
| Argon | Ar | 39.94 | 151 | 48.6 | 0.290 |
| Benzene | C ₆ H ₆ | 78.11 | 563 | 49.3 | 0.274 |
| Butane | C ₄ H ₁₀ | 58.12 | 425 | 38.0 | 0.274 |
| Carbon | C | 12.01 | — | — | — |
| Carbon dioxide | CO ₂ | 44.01 | 304 | 73.9 | 0.276 |
| Carbon monoxide | CO | 28.01 | 133 | 35.0 | 0.294 |
| Copper | Cu | 63.54 | — | — | — |
| Ethane | C ₂ H ₆ | 30.07 | 305 | 48.8 | 0.285 |
| Ethyl alcohol | C ₂ H ₅ OH | 46.07 | 516 | 63.8 | 0.249 |
| Ethylene | C ₂ H ₄ | 28.05 | 283 | 51.2 | 0.270 |
| Helium | He | 4.003 | 5.2 | 2.3 | 0.300 |
| Hydrogen | H ₂ | 2.018 | 33.2 | 13.0 | 0.304 |
| Methane | CH ₄ | 16.04 | 191 | 46.4 | 0.290 |
| Methyl alcohol | CH ₃ OH | 32.05 | 513 | 79.5 | 0.220 |
| Nitrogen | N ₂ | 28.01 | 126 | 33.9 | 0.291 |
| Octane | C ₈ H ₁₈ | 114.22 | 569 | 24.9 | 0.258 |
| Oxygen | O ₂ | 32.00 | 154 | 50.5 | 0.290 |
| Propane | C ₃ H ₈ | 44.09 | 370 | 42.7 | 0.276 |
| Propylene | C ₃ H ₆ | 42.08 | 365 | 46.2 | 0.276 |
| Refrigerant 12 | CCl ₂ F ₂ | 120.92 | 385 | 41.2 | 0.278 |
| Refrigerant 134a | CF ₃ CH ₂ F | 102.03 | 374 | 40.7 | 0.260 |
| Sulfur dioxide | SO ₂ | 64.06 | 431 | 78.7 | 0.268 |
| Water | H ₂ O | 18.02 | 647.3 | 220.9 | 0.233 |

Source: Adapted from *International Critical Tables* and L. C. Nelson and E. F. Obert, *Generalized Compressibility Charts, Chem. Eng.*, 61: 203 (1954).