

KE-107.3100 Process Simulation
Examination 28.10.2008; time: 13:00-16:00

-write your name & student no:

Theory (max.1h) : Answer in Finnish, Swedish or English

1. Explain shortly:
 - a) Rating b) Critical temperature c) Sequential modular simulator
2. Different types of reactor models in Pro/2
3. How to select VLE methods

Simulation part (2h): (Save each task in *prz and *out files and write your answers on paper)

1. Simulate a distillation column for separation of 20 t/h of propane and propene solution. Feed contains 50 w-% propane and 50 w-% of propene at 25 bar and 20 °C. 95 w-% propene is separated as distillate and 90 w-% propane is as bottom products. The column has 100 ideal trays.

- a) What is the column pressure if condenser temperature is 42 °C
- b) Calculate the diameter and height of the column with valve trays (efficiency 80%)

2. Simulate a propene refrigeration system. Propene at 40 °C, saturated liquid (9 t/h) is led to a flash tank F-1. The flash tank is at 400 kPa. Vapor from F-1 is compressed in C-1 to outlet pressure 1600 kPa and totally condensed in a heat exchanger E-1 with pressure drop 50 kPa and the saturated liquid is recycle to the same flash (F-1) via control valve. The saturated liquid from F-1 is feed to cold storage T-1. The cold storage tank contains saturated liquid at 105 kPa and has heat loss 50kW. The vapor vaporized in T-1 is fed via compressor C-2 to the flash tank (F-1) and the liquid from T-1 is taken out as product. (Compressor C-1 and C-2 are polytropic with efficiency 80%)

- a) What is the cold storage T-1 temperature?
- b) How much cooling water is needed in countercurrent E-1, if inlet and outlet temperature of water is 20 °C and 40 °C

3. Dimethyl ether (DME) can potentially be manufactured by two routes:

- i) from methanol: $2\text{CH}_3\text{OH} \rightarrow \text{CH}_3\text{OCH}_3 + \text{H}_2\text{O}$ or
- ii) from methanol and methane: $\text{CH}_3\text{OH} + \text{CH}_4 \rightarrow \text{CH}_3\text{OCH}_3 + \text{H}_2$

- a) Calculate which is the more potential route at 1500 kPa and 250 °C
- b) If maximum temperature of catalyst is 300 °C, calculate the adiabatic temperature rise for the chosen reaction and choose the reactor type.

Points: theory: 2p/each
simulation: 1). 3p, 2). 4p, 3). 3p and exercise attendance 4p.